

Hydrogen Generator For  
Hydrogen Desulfurization of Hydrocarbon Feeds

Cross Reference to Related Application

This is a continuation-in-part of U.S. patent application Serial  
5 No. 10/369,359 filed on February 18, 2003.

Technical Field

This invention relates to using a hydrogen generator, such as a small catalytic partial oxidizer (mini-CPO), a homogeneous, non-catalytic partial oxidizer (POX), an auto-thermal reformer (ATR), a catalytic steam reformer, or a small water hydrolyzer, to generate hydrogen-containing reformate as an input, along with natural gas, liquified petroleum gas, or other hydrocarbon fuels, for hydrogen desulfurization (HDS) in the production of hydrogen from hydrocarbon fuels, for use, for instance, in fuel cell power plants, refineries, or other processes.

Background Art

Fuel cell power plants use hydrogen as the fuel. Current technology includes conversion of hydrocarbon feeds to hydrogen by passing natural gas through a desulfurizer, a catalytic partial oxidizer (or other reformer), a water-gas shift reactor, and a preferential carbon monoxide oxidizer for the generation of significant hydrogen for use as a fuel in a fuel cell, in which hydrogen and oxygen on opposite sides of the electrolyte are converted to electricity and water, in the known fashion.

Referring to Fig. 1, hydrogen reformate is generated in a line 13 by a major reformer 14, such as a catalytic partial oxidizer (CPO), an auto-thermal reformer or a steam reformer, which in turn receives desulfurized hydrocarbon fuel, such as natural gas, over a line 16  
5 from a hydrogen desulfurizer 17. The hydrogen desulfurizer 17 receives hydrocarbon fuel over a line 19. The CPO 14 also receives humidified air, from a suitable source such as an enthalpy recovery device, over a line 23. In the CPO 14, the hydrocarbons in the fuel react with the humidified air on a catalyst, such as rhodium, iridium or zirconia, to produce in the line 13 reformate which, for methane feedstock, is roughly 37% hydrogen, 14% CO, 4% CO<sub>2</sub> and traces of other gases, which is further processed with water from a line 24  
10 in a water-gas shift reactor 26 and a preferential CO oxidizer 27 to make it suitable for use as fuel in a line 31, such as for a fuel cell.  
15

However, the hydrogen desulfurizer requires hydrogen enrichment in order to convert sulfur compounds, such as thiophene, into hydrogen sulfide, which is captured on adsorbents, such as zinc oxide. This hydrogen is provided by a hydrogen recycle blower 30 which pressurizes hydrogen from a line 31 and applies it over a line  
20 32 to the hydrogen desulfurizer 17. A plurality of valves 34 allow adjustment of the processes, all as is known.

Problems with this system include the fact that the hydrogen blower 30 is expensive, and it consumes on the order of 2 kW of the power generated by the fuel cell for a 150 kW fuel cell power plant.  
25 Additionally, there is a significant amount of steam present in the hydrogen recycle stream 32 which has a negative impact on the hydrogen sulfide adsorption on zinc oxide in the hydrogen desulfurizer 17. This can impair the reduction of the level of sulfur, which must

reach the parts-per-billion (ppb) level for fuel cell applications and to avoid rapid deactivation of catalysts used in the process.

#### Disclosure of Invention

Objects of the invention include providing hydrogen to a hydrogen desulfurizing unit: which has less humidity in it than is provided by hydrogen recycled from a reformate stream, which does not require equipment costing several thousand dollars, and which requires substantially no energy for operation; and provision of: improved hydrogen generation, such as for fuel in a fuel cell; a lower cost source of hydrogen-containing reformate; and reduced parasitic power in a fuel cell power plant utilizing hydrogen-containing reformate.

This invention is predicated on the discovery that the higher temperature in a hydrogen desulfurizer, which results from using hydrogen generated in a mini-reformer, prevents the carbon monoxide in the reformer product from having any significant adverse effect on the precious metal catalyst (such as platinum) or the adsorption material (such as zinc oxide) in a hydrogen desulfurizer.

According to the present invention, hydrocarbon feed (such as natural gas) and air are fed to a small hydrogen generator to generate hydrogen rich reformate to be fed to a hydrogen desulfurizer, thereby eliminating the need for a hydrogen recycle blower. The invention reduces cost, power consumption and moisture in the hydrogen gas provided to a hydrogen desulfurizer.

According to the invention further, the small hydrogen generator is run in a nearly steady state condition, obviating the need for controls; any excess hydrogen that is generated simply becoming part of the fuel stream, which is economically utilized.

By providing dry reformate to the hydrogen desulfurizer, the adsorption of sulfur on the zinc oxide is enhanced, reducing sulfur to the parts per billion level, which is significant. The invention also provides a certain amount of heat which raises the desulfurizing 5 process from about 260°C (500°F) to about 350°C (662°F), thereby to aid in the desulfurizing process.

According to the invention, the hydrogen generator may be a small catalytic partial oxidizer (mini-CPO), a homogeneous non-catalytic partial oxidizer (mini-POX), a small auto-thermal reformer 10 (mini-ATR), a small catalytic steam reformer, a small water electrolyzer, or any other unit that produces hydrogen suitable for use in hydrogen desulfurization, particularly any unit that produces dry hydrogen at an elevated temperature with no parasitic cost or loss of efficiency.

15 Other objects, features and advantages of the present invention will become more apparent in the light of the following detailed description of exemplary embodiments thereof, as illustrated in the accompanying drawing.

#### Brief Description of the Drawings

20 Fig. 1 is a simplified schematic illustration of a hydrogen desulfurizer feeding a major reformer, with recycled hydrogen gas being provided through a hydrogen blower to the hydrogen desulfurizer, as known in the prior art.

25 Fig. 2 is a simplified schematic diagram of a hydrogen desulfurizer being supplied hydrogen rich reformate generated by a mini-CPO, in accordance with the present invention.

Figs. 3 and 4 are partial, simplified schematic diagrams of the embodiment of Fig. 2 except using a mini-POX and a mini-ATR, respectively.

#### Mode(s) for Carrying Out the Invention

5 Referring to Fig. 2, a mini-reformer, such as a mini-CPO 36, about the size of a 12 ounce beverage can, receives humidified air through a valve 37 and receives hydrocarbon fuel, such as natural gas, through a fixed orifice 38. The multiplicity of valves and the fixed orifice allows adjusting the correct flows to the mini-CPO, the  
10 hydrogen desulfurizer and the major reformer. In the mini-CPO, the fuel, which for natural gas, is typically more than 99% methane with traces of sulfur compounds, nitrogen and other hydrocarbons, is converted, along with the humidified air, to reformat, which may comprise roughly 30% hydrogen, 12% CO, and small amounts of  
15 other gases such as CO<sub>2</sub> and H<sub>2</sub>O, nitrogen from the humidifier, and unconverted hydrocarbons.

The reformat produced by the mini-CPO 36 in a line 38 is mixed with the fuel at the inlet to the hydrogen desulfurizer 17. Since no water is applied to the mini-CPO, the reformat is much  
20 drier than the reformat generated in the line 31 by the water-shift reactor 26 and preferential CO oxidizer 27 which provides significant humidity in the reformat in the line 31. Thus, a drier reformat is provided (about 2.8 mol % steam from the mini-CPO compared with about 8.8 mol % steam in the prior art) to the hydrogen desulfurizer,  
25 which enhances the adsorption on zinc oxide and helps to reduce the sulfur to the parts per billion level.

Although there is carbon monoxide in the CPO reformat, the heat input from the mini-CPO helps the hydrogen desulfurizer to run

at between 650°F (343°C) and 750°F (400°C); these temperatures are high enough so that the carbon monoxide has only a relatively small negative effect on the desulfurizer catalyst. Thus, a further benefit of the present invention is that it provides some heat to  
5 enhance the desulfurization process.

The small hydrogen generator in the embodiment of Fig. 2 is a mini-CPO. However, the small hydrogen generator may be a mini-POX 36a as illustrated in Fig. 3, a mini-ATR 36b as illustrated in Fig. 4, or it may be a small catalytic steam reformer, a small water  
10 electrolyzer, or any other type of hydrogen generator that will produce hydrogen.

The small hydrogen generator may operate with dry air, if desired, although humidified air is presently thought to be preferable. The major reformer 14 may be a CPO, a catalytic steam reformer, or  
15 an autothermal reformer. The invention may be used in desulfurization processes for other than fuel cell power plants, such as in a refinery, or even in futuristic fuel (e.g., gasoline) stations.

Because the use of the small hydrogen generator will increase the temperature at the inlet to the hydrogen desulfurizer, the  
20 hydrogen generator may be configured with several layers of adsorbent material interspersed with several layers of precious metal hydrogen desulfurizing catalyst material so that the adsorbent may be replaced regularly, without either discarding or sorting through the catalyst to reclaim it, as is disclosed in copending U.S. patent  
25 application Serial No. 10/386,317, filed March 11, 2003.

Although the invention is well suited to provide hydrogen-rich reformate fuel for fuel cells, it may be used in refineries for desulfurization of all types of hydrocarbon fuels, such as natural gas,

liquified petroleum gas, gasoline, diesel (including JP-8), kerosene, and other fuels generated from biomass and the like.

Although the embodiment described herein is used in the desulfurization of natural gas, it may also be used in the  
5 desulfurization of other hydrocarbon feeds such as liquified petroleum gas, gasoline, diesel fuel, methane, and the like.

Thus, although the invention has been shown and described with respect to exemplary embodiments thereof, it should be understood by those skilled in the art that the foregoing and various  
10 other changes, omissions and additions may be made therein and thereto, without departing from the spirit and scope of the invention.

We claim: